


**注意：考試開始鈴響前，不得翻閱試題，  
並不得書寫、畫記、作答。**

國立清華大學 108 學年度碩士班考試入學試題

系所班組別：核子工程與科學研究所 甲組

考試科目(代碼)：流體力學(3204)

### —作答注意事項—

1. 請核對答案卷(卡)上之准考證號、科目名稱是否正確。
2. 作答中如有發現試題印刷不清，得舉手請監試人員處理，但不得要求解釋題意。
3. 考生限在答案卷上標記「由此開始作答」區內作答，且不可書寫姓名、准考證號或與作答無關之其他文字或符號。
4. 答案卷用盡不得要求加頁。
5. 答案卷可用任何書寫工具作答，惟為方便閱卷辨識，請儘量使用藍色或黑色書寫；答案卡限用 2B 鉛筆畫記；如畫記不清(含未依範例畫記)致光學閱讀機無法辨識答案者，其後果一律由考生自行負責。
6. 其他應考規則、違規處理及扣分方式，請自行詳閱准考證明上「國立清華大學試場規則及違規處理辦法」，無法因本試題封面作答注意事項中未列明而稱未知悉。

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共 4 頁，第 1 頁

\*請在【答案卷】作答

1. (20%)

- (1) Please define the friction factor for pipe flow.
- (2) Please explain the dependence of friction factors for the laminar flow and turbulent flow on the surface roughness.
- (3) Plot the Moody diagram and explain it as possible as you can.

2. (15%)

As shown in Fig. 1, the fluid velocity along the streamline is  $\vec{V} = V\vec{s}$ .

The acceleration can be expressed as

$$\vec{a} = \frac{d\vec{V}}{dt} = a_s\vec{s} + a_n\vec{n}$$

Please prove

$$a_s = V \frac{dV}{ds} \quad \text{and} \quad a_n = \frac{V^2}{R}$$

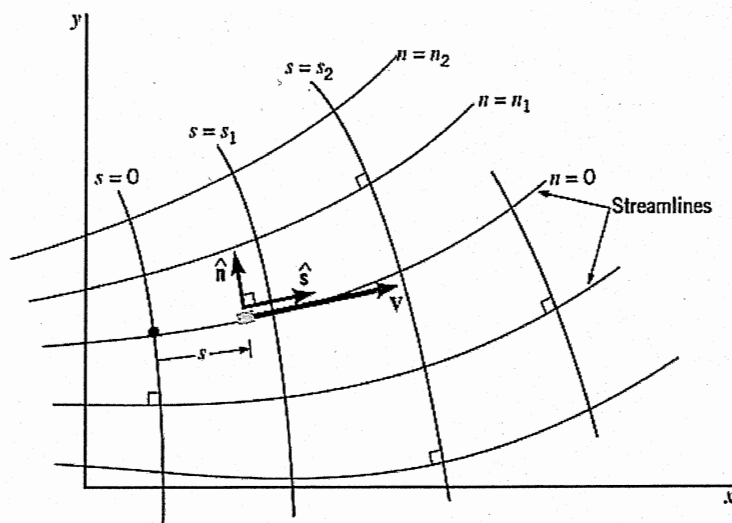


Figure 1

國立清華大學 108 學年度碩士班考試入學試題

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3. (20%)

Consider steady, incompressible, laminar flow of a Newtonian fluid in an infinitely long round pipe annulus of inner radius  $R_i$  and outer radius  $R_o$  (as shown in Fig. 2). Ignore the gravity effect. A constant negative pressure gradient  $\partial p / \partial x$  is applied in the x-direction,

$$\frac{\partial p}{\partial x} = \frac{(P_2 - P_1)}{(x_2 - x_1)}$$

Derive an expression for the velocity field in the annular space in the pipe.

Hint:

The velocity field is axisymmetric with no swirl, implying that  $u_\theta = 0$  and

$$\frac{\partial}{\partial \theta} = 0$$

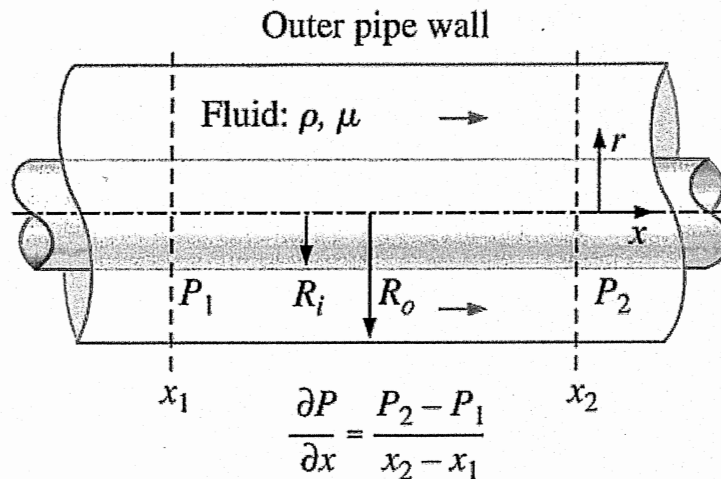


Figure 2

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共\_4\_頁，第\_3\_頁 \*請在【答案卷】作答

4. (25 %)

As the fluid with the velocity of  $U$  passes over a flat plate with the length of  $L$  (shown in Fig. 3), the boundary layer is laminar for a short distance downstream from the leading edge. In this flow condition, we consider a steady two dimensional laminar flow with negligible gravitational effect. The governing equations can be reduced to the followings. ( $\delta$  is the boundary layer thickness)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \frac{\mu}{\rho} \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

Simplify above equations into the Boundary layer equation (as shown below) using the dimensional analysis. In addition, please find the relationship of boundary thickness and Reynolds number.

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}$$

Hint : (1)  $L \gg \delta$

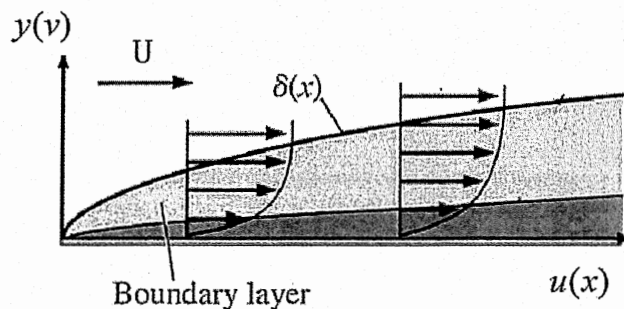


Figure 3

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5. (20 %)

A liquid of density  $\rho$  and viscosity  $\mu$  flows by gravity through a hole of diameter  $d$  in the bottom of a tank of diameter  $D$  (Fig. 4). At the start of the experiment, the liquid surface is at height  $L$  above the bottom of the tank, as sketched. The liquid exits the tank as a jet with average velocity  $U$  straight down as also sketched. Using dimensional analysis of Buckingham Pi Theorem, generate a dimensionless relationship for  $V$  as a function of the other parameters in the problem. Identify any established nondimensional parameters that appear in your results.

(Hint: There are three length scales in this problem. For consistency, choose  $L$  as your length scale.)

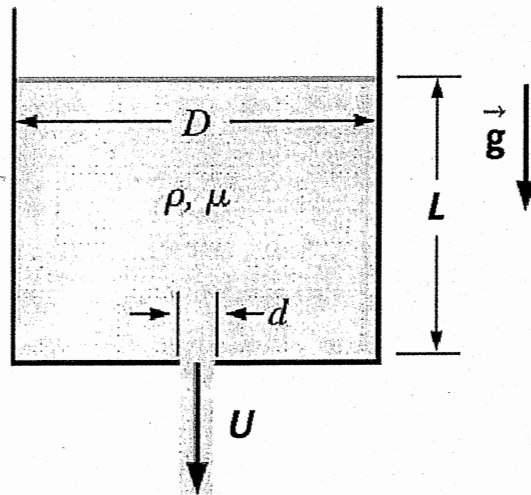


Figure 4