

注意：考試開始鈴響前，不得翻閱試題，
並不得書寫、畫記、作答。


國立清華大學 114 學年度碩士班考試入學試題

系所班組別：化學工程學系

科目代碼：1002

考試科目：化工熱力學及化學反應工程

—作答注意事項—

1. 請核對答案卷（卡）上之准考證號、科目名稱是否正確。
2. 考試開始後，請於作答前先翻閱整份試題，是否有污損或試題印刷不清，得舉手請監試人員處理，但不得要求解釋題意。
3. 考生限在答案卷上標記「由此開始作答」區內作答，且不可書寫姓名、准考證號或與作答無關之其他文字或符號。
4. 答案卷用盡不得要求加頁。
5. 答案卷可用任何書寫工具作答，惟為方便閱卷辨識，請儘量使用藍色或黑色書寫；答案卡限用 2B 鉛筆畫記；如畫記不清（含未依範例畫記）致光學閱讀機無法辨識答案者，其後果一律由考生自行負責。
6. 其他應考規則、違規處理及扣分方式，請自行詳閱准考證明上「國立清華大學試場規則及違規處理辦法」，無法因本試題封面作答注意事項中未列明而稱未知悉。

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Problem 1 (10%)

Consider a binary A - B system in vapor/liquid equilibrium. At a constant pressure of 1 atm, the boiling point of A is 300°C , and that of B is 400°C . The vapor phase is an ideal solution. The Gibbs energies of pure A and pure B in the vapor phase are $\Delta G_A^{o,gas}$ and $\Delta G_B^{o,gas}$, respectively.

- (a) (2%) What is the enthalpy change of mixing of the vapor phase?
- (b) (2%) What is the Gibbs energy change of mixing of the vapor phase?
- (c) (3%) What is the partial Gibbs energy of A , \bar{G}_A^{gas} , in the vapor phase?
- (d) (3%) The A - B binary system is an isomorphous system. It has an azeotrope at 220°C and 60.0at.% A -40.0at.% B . Draw a binary A - B temperature-composition (T - x) phase diagram with a temperature range from 100°C to 600°C , and label all the phase regions.

Problem 2 (10%)

Consider a binary A - B system in liquid/solid equilibrium. At a constant pressure of 1 atm, the melting point of A is 300°C , and that of B is 400°C . The A - B binary system is isomorphous at higher temperatures, and at temperatures lower than 220°C exhibits a miscibility gap with a critical concentration at 60 at.% A -40 at.% B .

- (a) (3%) Draw a binary A - B temperature-composition (T - x) phase diagram with a temperature range from 100°C to 600°C , and label all the phase regions.
- (b) (2%) Draw a schematic Gibbs energy-composition (G - x) diagram showing both the liquid phase and the solid phase at 350°C .
- (c) (3%) Draw a schematic Gibbs energy-composition (G - x) diagram showing both the liquid phase and the solid phase at 200°C .
- (d) (2%) Is the solid solution an ideal solution? Why or why not?

Problem 3 (20%)

In thermodynamics, the isothermal compressibility quantifies the instantaneous relative change in volume of a material in response to a change in pressure. Mathematically, isothermal compressibility β is expressed as:

$$\beta = -\frac{1}{V} \left(\frac{\partial V}{\partial p} \right)_T$$

where V , p , and T are volume, pressure, and temperature, respectively.

- (a) (5%) Derive the expression of β for the ideal gas as a function of p .

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(b) (10%) A liquid A exhibits a constant isothermal compressibility β over a pressure range from p_1 to p_2 . Show that the reversible isothermal work w required to compress liquid A from an initial volume V_1 , (at a pressure p_1) to a final volume V_2 (at a pressure p_2) is given by:

$$w = -p_1(V_2 - V_1) + \frac{V_1}{\beta} \left(\frac{V_2}{V_1} \ln \frac{V_2}{V_1} - \frac{V_2}{V_1} + 1 \right)$$

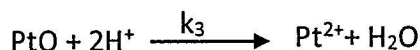
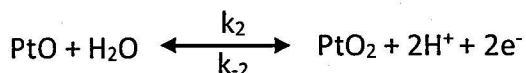
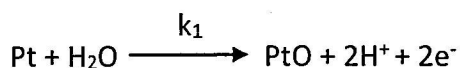
(c) (5%) Following (b), it can be shown that if β is small (incompressible fluid), the w can be approximated as:

$$w \approx \frac{\beta V_1}{2} (p_2^2 - p_1^2)$$

Using this equation, calculate the work required to compress one mole of liquid A reversibly and isothermally from 1 bar to 10 bar at 300 K. Take the value of β to be 10^{-5} bar^{-1} and the molar volume to be 10^{-1} L/mol at 300 K.

Problem 4 (10%)

Assuming platinum (Pt) oxidation and dissolution impedes the durability of hydrogen fuel cells, especially under very low electrode loading. Modeling Pt oxidation and dissolution in a fuel cell cathode is therefore very important. Assuming the oxidation and dissolution of Pt follows the reactions below



where $k_1 = 1$, $k_2 = 3$, $k_{-2} = 5$, and $k_3 = 4$.

As a chemical engineer, you are expected to use the provided information to model the oxidation and dissolution of Pt over time.

(a) (3%) List down the differential equations to model the dynamic changes of Pt-containing species.

(b) (7%) The Pt on the electrode was originally pure metallic. Assuming that water, protons, and electrons are in excess, how does the content of PtO change with time?

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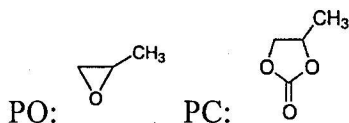
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(Please derive the PtO content as a function of time)

Problem 5 (10%)

Carbon capture and utilization is an attractive way of providing economic incentives to drive efforts in converting waste CO₂ into value added chemicals. The conversion of CO₂ and propylene oxide (PO) into propylene carbonate (PC) is a route considered by many chemical companies.

Species	Formation Enthalpy (kJ/mol)	Entropy at 1 bar (J/mol/K)
CO _{2(g)}	-393.51	213.8
PO _(g)	-94.68	287.4
PC _(l)	-613	218.6
H ₂ O _(l)	-285.83	69.95



- (a) (5%) Calculate the equilibrium constant of the reaction of CO₂ and PO to form PC at 180 °C.
- (b) (5%) Calculate the equilibrium conversion at 180 °C if the reactor is initially fed with a CO₂-to-PO ratio of 1.

Problem 6 (20%)

The elementary irreversible gas phase reaction 2A → B is carried out in a constant volume batch reactor where 50 % conversion is achieved in 1 hour. Pure A is charged to the reactor at an initial concentration of 0.2 mol/dm³. If the same reaction is carried out in a CSTR, what volume would be necessary to achieve 50 % conversion for a feed molar flow rate of 500 mol/h and an entering concentration of A of 0.2 mol/dm³?

Problem 7 (20%)

(20%) A mixture containing 28% SO₂ and 72% air (comprising 21% O₂ and 79% N₂) is introduced into a flow reactor, where it undergoes gas-phase oxidation under constant isothermal and isobaric conditions.



- (a) (10%) Please show the concentrations SO₂, SO₃, O₂, and N₂ as functions of

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conversion for the case when the total pressure is 1485 kPa and the temperature is constant at 500 K.

(b) (10%) Please create a plot showing the concentrations of SO_2 , SO_3 , O_2 , and N_2 as functions of conversion ($X = 0, 0.25, 0.5$, and 1).