

1. Water is compressed from state (1) to state (5). Shown as in Fig. 1. Assume the specific volume of water v_f and its volume expansivity α_p are constant. Water in liquid phase is following the state equation $P=A\ln T$, where A is constant, and the steam in vapor phase is following the state equation $P(v-b)=RT$, where b is constant. The heat capacity of water is constant; $C_{p(l)}$, and the heat capacity of steam is constant too; $C_{p(v)}$. Given the saturated liquid enthalpy at state(3); $h_{f,3}$, and the saturated vapor enthalpy at state (3'), $h_{g,3}$, P_1, P_2, P_3 , are the isobaric lines, $T_4=T_5, T_3=T_{3'}$. Define volume expansivity:

$$\alpha_p = \frac{1}{v_f} \left(\frac{\partial v_f}{\partial T} \right)_p$$

- (a) Please evaluate enthalpy change Δh_{12} (2%) and Δh_{22} (7%) and entropy change ΔS_{12} (2%) and ΔS_{22} (4%) with function of $C_{p(l)}, T_1, T_2, T_2', P_1, P_2, \alpha_p, v_f$ and A .
- (b) Evaluate the enthalpy change $\Delta h_{33'}$ and entropy change $\Delta S_{33'}$ from state (3) to state (3') with function of $h_{f,3}, h_{g,3}$, and T_3 (5%)
- (c) Evaluate the enthalpy change $\Delta h_{3'4}$ and the entropy change $\Delta S_{3'4}$ from state (3') to state (4) with function of $C_{p(v)}, T_3$ and T_4 (6%)
- (d) Evaluate the enthalpy change Δh_{45} and the entropy change ΔS_{45} from state (4) to state (5) with function of R, b, P_2 and P_3 (4%)

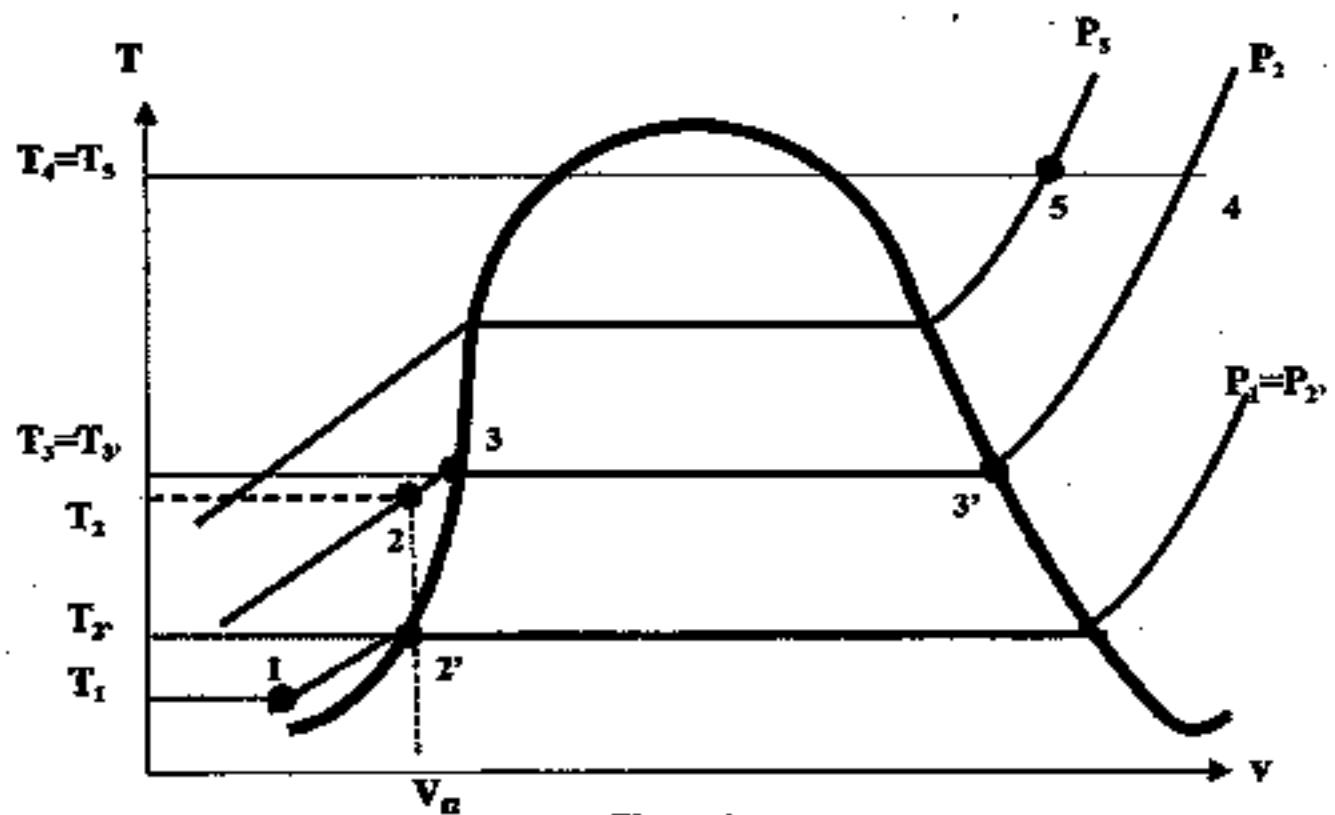
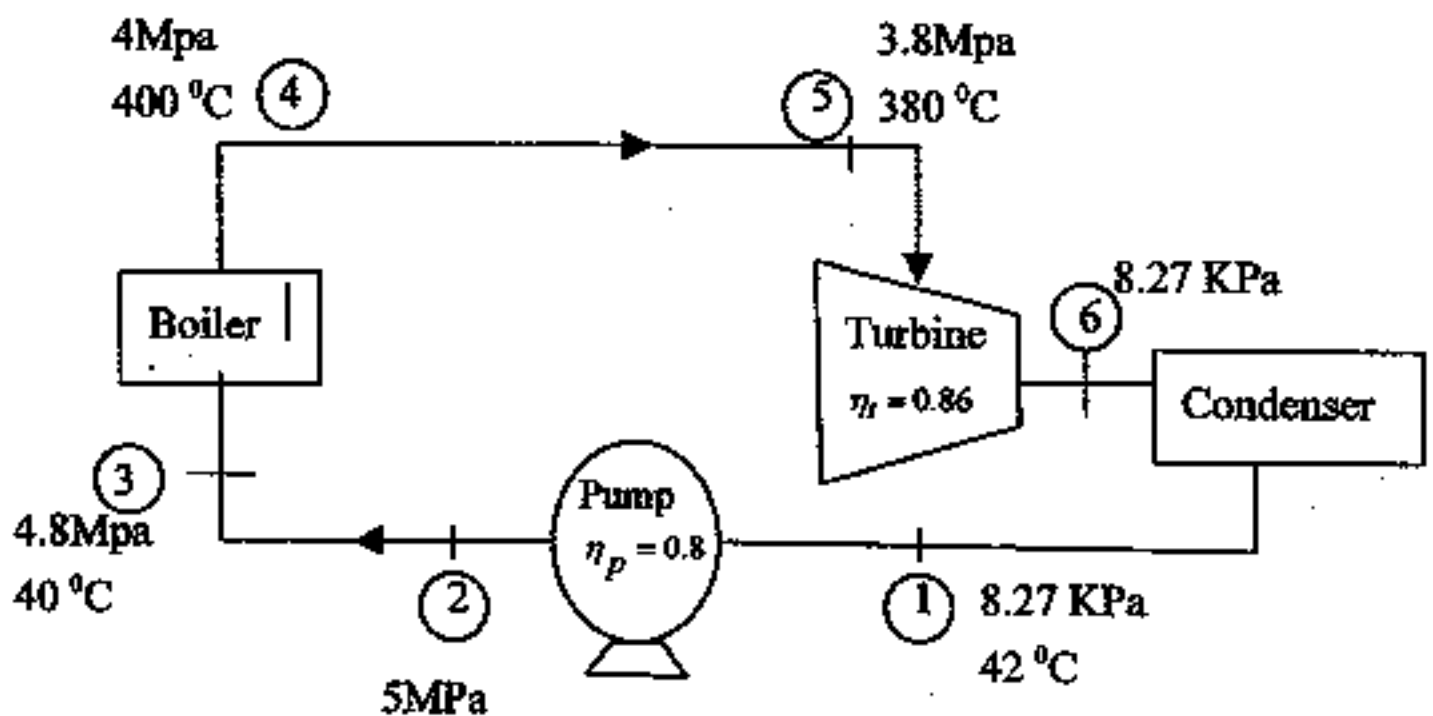


Figure 1

2. A steam power plant operates on a cycle with pressure and temperatures as designed in following figure. The efficiency of the turbine is 86% and the efficiency of the pump is 80%. Determine
- The isentropic pump work W_{ps} (2%), The actual pump work W_a (2%)
 - The enthalpy of state 2 (2%)
 - The temperature of state 2, T_{2s} , if the pump working as the reversible and adiabatic (isentropically) process (2%)
 - The actual temperature of state 2, T_2 (2%)
 - The entropy of state 2, S_2 (2%)
 - The quality of state 6, X_{6s} (2%) and The enthalpy of state 6, h_{6s} (2%), if the turbine working as the reversible and adiabatic (isentropically) process
 - The actual turbine work W_t (2%), The actual enthalpy of state 6, h_6 (2%)
 - The actual quality of state 6, X_6 (2%), The actual entropy of state 6, S_6 (2%)
 - The net work of cycle W_{net} (2%), The heat input of the boiler q_H (2%)
 - The thermal efficiency of the cycle η (2%)



State (Unit)	T (°C)	P (Mpa)	V_f (m ³ /Kg)	V_g (m ³ /Kg)	U_f (KJ/Kg)	U_g (KJ/Kg)	h_f (KJ/Kg)	h_g (KJ/Kg)	S_f (KJ/Kg·°K)	S_g (KJ/Kg·°K)
Superheat	380	3.8		0.0741		2877.3		3158		6.7159
Superheat	400	4.0		0.07341		2919.6		3213.6		6.769
Saturated	40	7.38×10^{-3}	0.00108	19.52	167.56	2430.1	167.57	2574.3	0.5725	8.257
Saturated	42	8.27×10^{-3}	0.001	17.4	178	2433	178.01	2578.7	0.6057	8.2109
Saturated	46	10×10^{-3}	0.001	14.67	191.82	2437.9	191.83	2584.7	0.6493	8.1502
Saturated	262	4.8	0.00128	0.04	1138.2	2597.86	1146.5	2795.3	2.9	5.987
Subcooled	40	5	0.001		166.95		171.97		0.5705	
Subcooled	60	5	0.00101		250.23		255.3		0.8285	

3. Explain the followings, and also give two thermodynamic properties as the examples for each of the four cases.
 - (a) State function (5%)
 - (b) Non-state function (path function) (5%)
 - (c) Intensive properties (5%)
 - (d) Extensive properties (5%)
4. Show that any flow of heat between two heat reservoir at temperature T_H and T_C where $T_H > T_C$, must be from the hotter to the cooler reservoir. (5%)
5. Please draw the T-S diagram for the ideal Carnot Cycle (5%) and calculate the cycle efficiency if the cycle is operating between high temperature reservoir T_H and low temperature reservoir T_L . (10%)